

Optimization of Heater Zone Layout for a Rotating Susceptor in a Cold-wall MOCVD Reactor

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❑ Metal-organic Chemical Vapor Deposition (MOCVD)

- CVD with metal-organic precursors (e.g., tri-methyl gallium)
- Used to manufacture Light Emitting Diodes (LEDs)

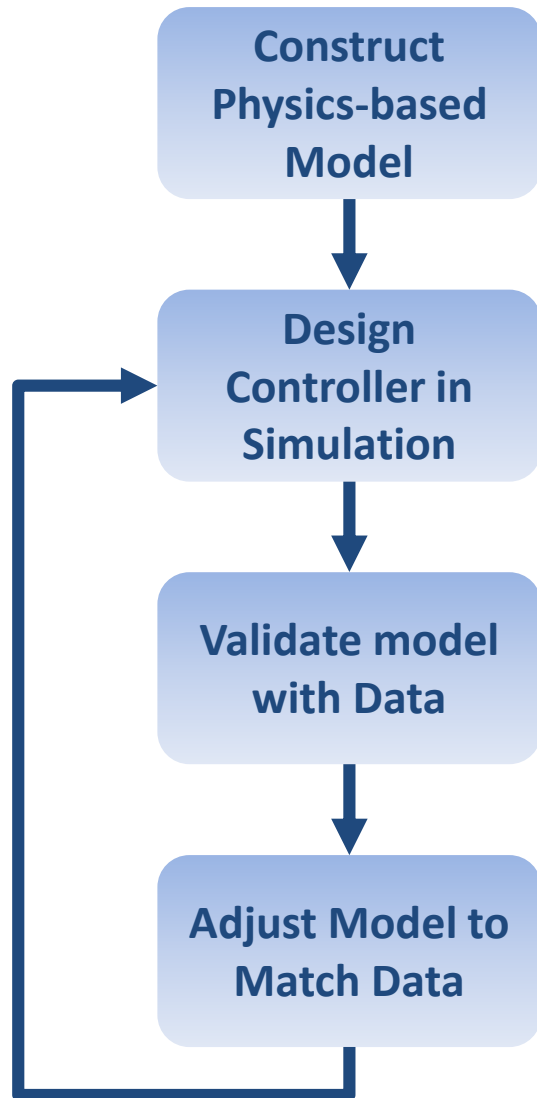
❑ A Case Study of Temperature Control of a Rotating Susceptor CVD Reactor

- Describes our Model-Based Control (MBC) approach using modeling, optimization and, control tools.
- Evaluate design limits for a range of operating conditions.

❑ Summary

Physical Model-Based Control

Design Process



Advantages

Modeling for Control Design

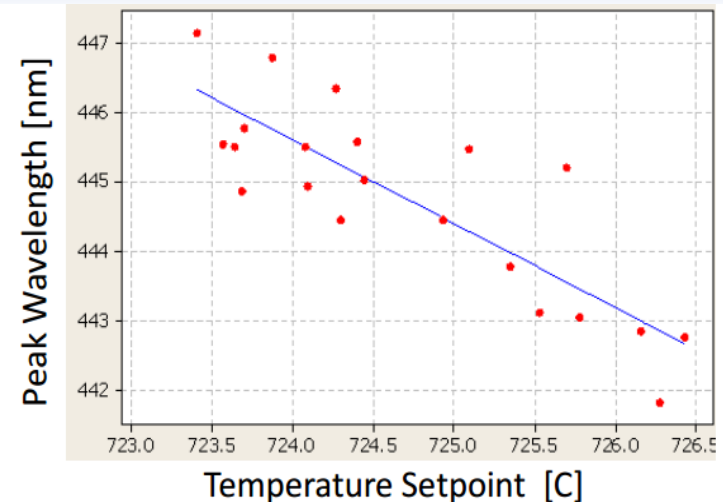
- Controller is tested in simulation for wide range of conditions.
- Much of the control design can be done without access to equipment.
- Ability to do controller development in parallel with chamber development.

Modeling for Equipment Design

- A model of the system that can be modified for “what-if” studies.
- Provides a tool for troubleshooting.
- Path for continued improvement.

MOCVD for LEDs

- ❑ MOCVD is used to produce Light Emitting Diodes (LEDs) by reacting metal-organic precursors (e.g., tri-methyl gallium, tri-methyl indium, etc.).
- ❑ Increasingly important for many applications (LED TV's, Lighting, etc.) due to potential for high efficiency.
- ❑ InGaN/GaN multiple quantum well (MQW) structures are grown on sapphire substrates for green, blue, and white LEDs.
- ❑ Studies* have shown that LED properties such as photoluminescence and electroluminescence can vary by a *factor of two* if the substrate temperature is changed from 1000°C to 1030°C.
- ❑ Involves many process steps over a wide temperature range (500-1100°C).
- ❑ As a result, *real-time control* of substrate temperature to within 1°C or less is essential for repeatable manufacturing of LEDs with *desired color*.



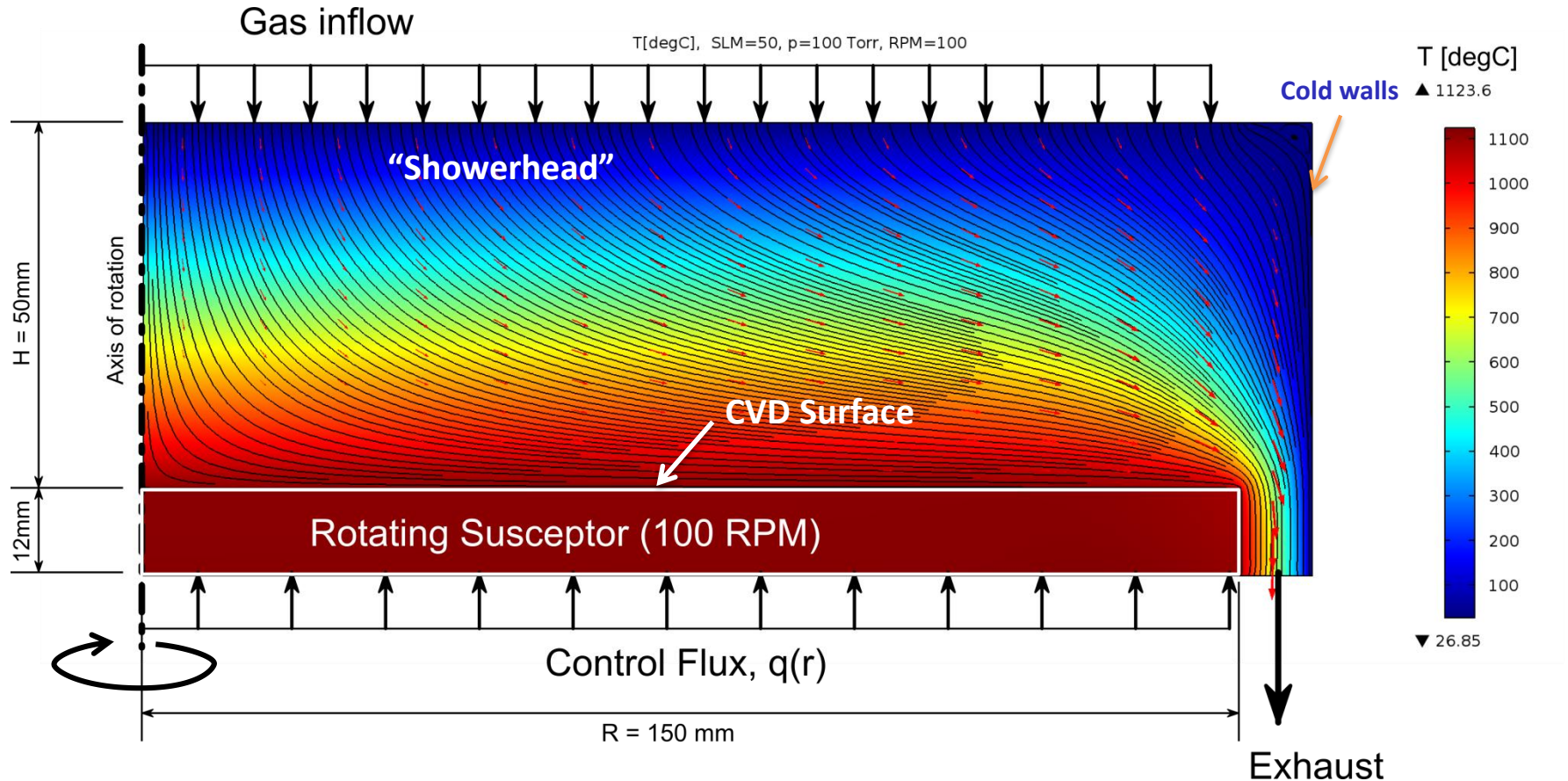
W. E. Quinn, *Driving Down HB-LED Costs: Implementation of Process Simulation Tools and Temperature Control Methods for High Yield MOCVD Growth*, Final Technical Report DoE Grant DE-EE0003252, p. 2012

* For example, see J. W. Ju, *et al.*, "Effects of p-GaN Growth Temperature on a Green InGaN/GaN Multiple Quantum Well," Journal of the Korean Physical Society, Vol. 50, No. 3, March 2007, pp. 810-813.

Finite Element (FEM) Model

A vertical reactor with top-side showerhead and rotating susceptor.

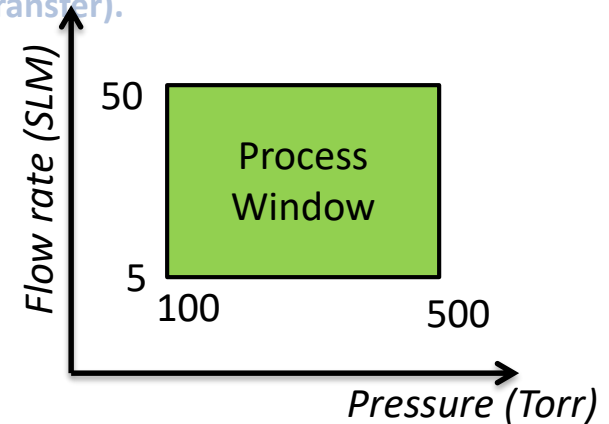
2D Axisymmetric FEM model – Non-isothermal flow, with swirl and buoyancy.



The temperature on the CVD Surface is critically important

Example Operating Conditions

- ❑ Hydrogen is the main carrier gas (no reactions, only heat transfer).
- ❑ Nominal operating temperature is 1100°C.
- ❑ Susceptor rotation rate = 100 RPM
- ❑ Operating pressure range is 100 Torr $\leq p \leq$ 500 Torr (1 Atm = 760 Torr)
- ❑ Operating flow rate range is 5 slm $\leq Q \leq$ 50 slm (slm = standard liters per minute)
- ❑ Required temperature uniformity of $\pm 0.5^\circ\text{C}$ (over widest possible area of susceptor)



The goal is to adjust the control flux, $q(r)$, to get good temperature uniformity on the CVD Surface.

Heat Transfer

❑ Gas Convection and Conduction

- The cold gas (27°C) is injected at the showerhead.
- Convective cooling flux of the susceptor is of order 10^4 W/m^2 .
- $q_c = h(T_{\text{sus}} - T_{\text{wall}})$, h is of order $10\text{-}100 \text{ W/m}^2\text{°C}$.

❑ Radiation

- $q_r = \varepsilon \sigma (T_{\text{sus}}^4 - T_{\text{wall}}^4)$, ε = effective emissivity, σ = Stefan-Boltzmann constant.
- Radiation losses are of order 10^5 W/m^2 .
- Radiation does not vary with flow rate or pressure.

❑ Conduction

- Gas conduction is fairly high for Hydrogen (compared to other gases).
- Solid conduction in susceptor is important since we heat from backside.

❑ The distribution of heat transfer at the CVD surface varies with flow rate and pressure due to changes in convection heat transfer.

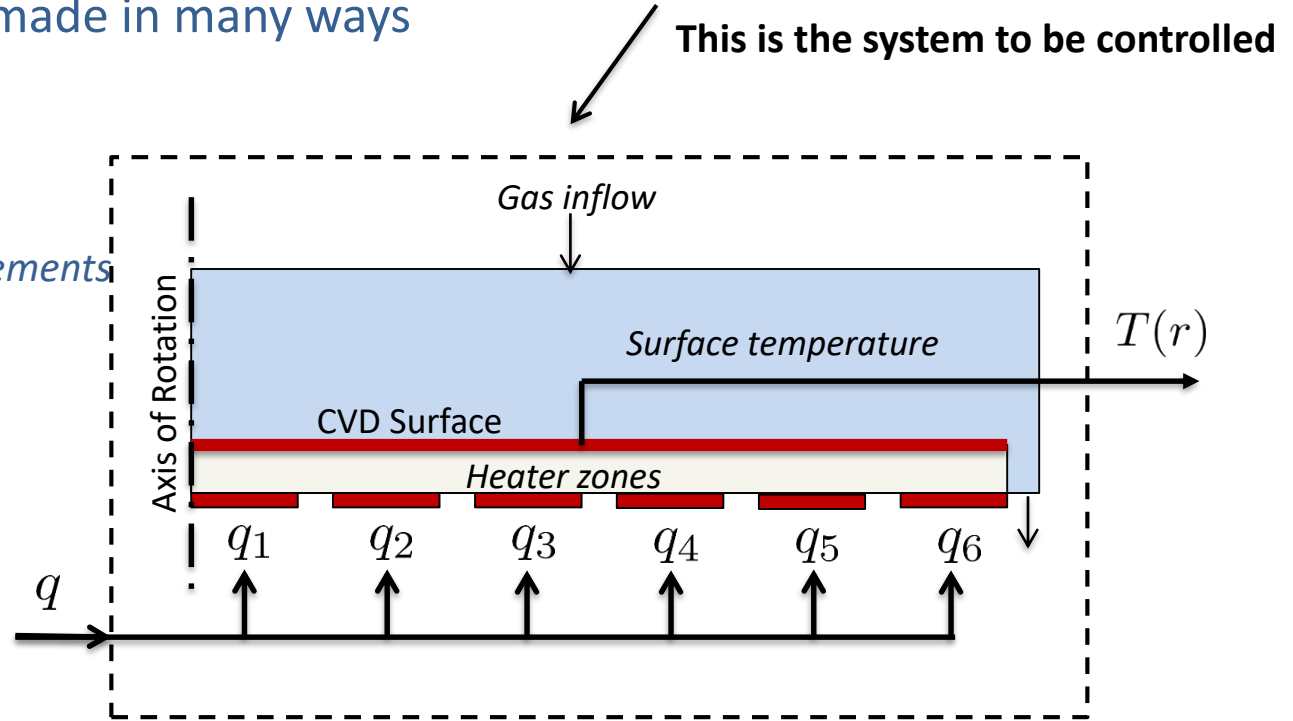
Heater Zone Definition

❑ It is common to divide the control flux into a number of independently controlled “zones”.

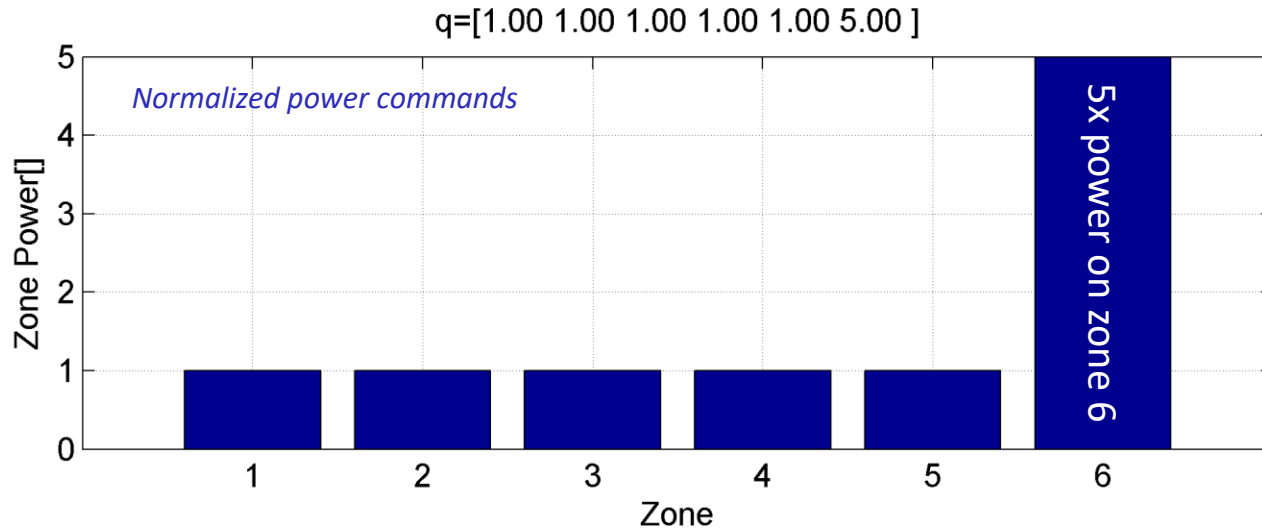
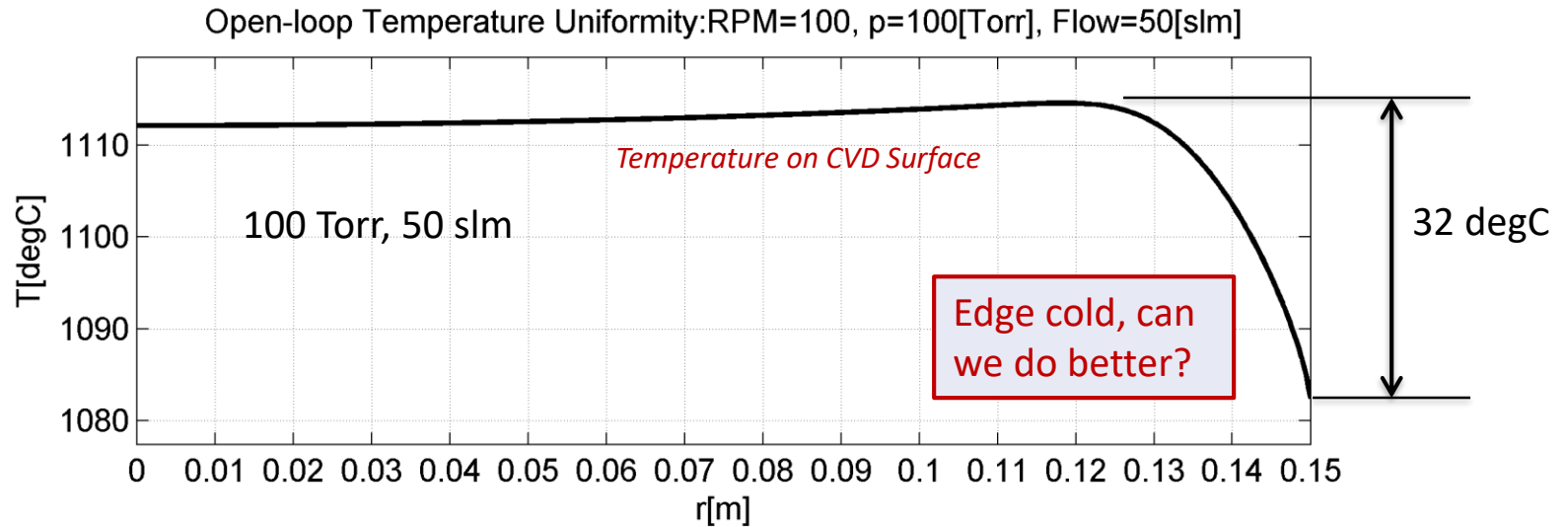
❑ Here we divide the control flux into six independent zones.

- Uniformly divided along the radius
- Heaters can be made in many ways

- *Resistive films*
- *Lamp arrays*
- *Hot filaments*
- *RF Inductive elements*



Baseline System Performance



Optimal Control

In words:

- Find the input control flux, q , for each heater that produces the best temperature uniformity.
- subject to the constraint that $q \geq 0$.
- the uniformity is optimized over limited radius ($r < R_{\max}$).

Mathematically:

$$q_{\text{opt}} = \arg \min_q ||T_{\text{ref}} - T(r, q)||$$

$$s.t. \quad q \geq 0$$

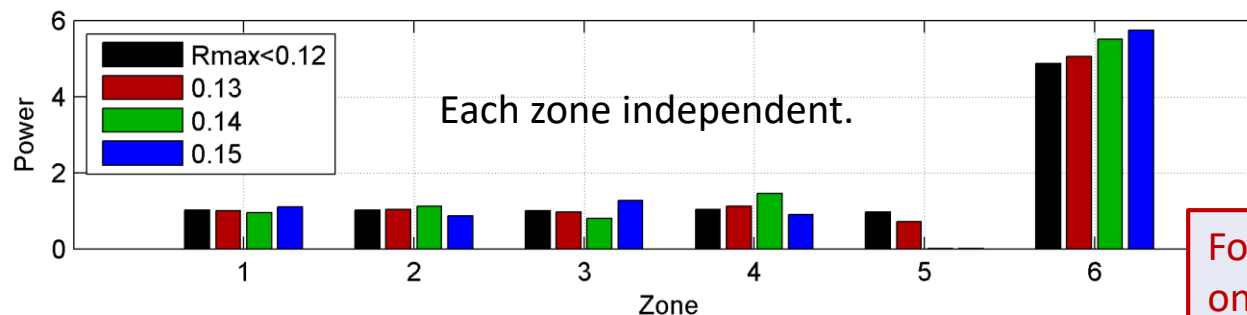
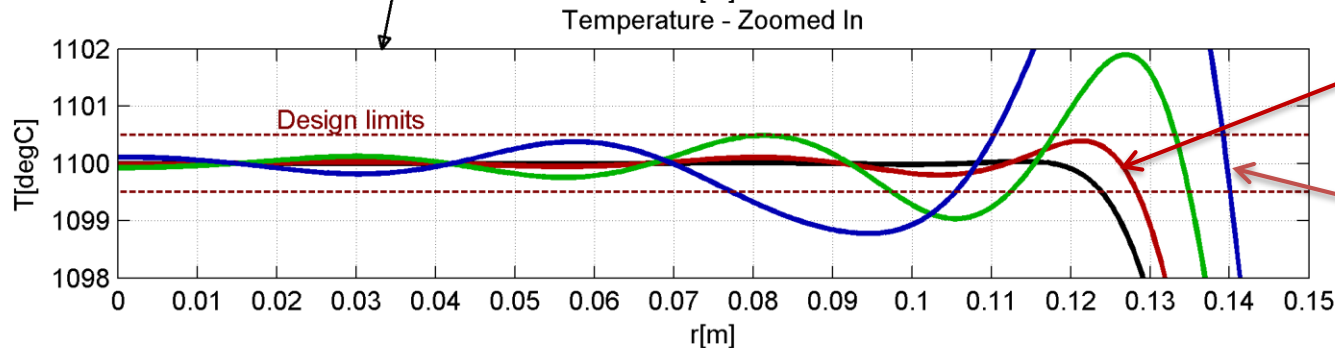
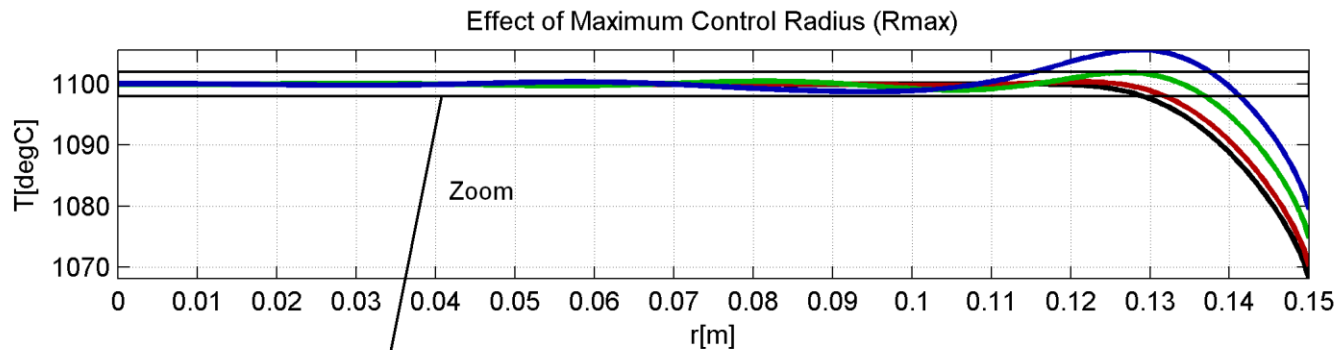
$$0 \leq r \leq R_{\max}$$

How Many Independent Heaters do we Need?

- ❑ In practice, for each independent heater we need additional power supply and additional temperature sensor which is **expensive**. We want as few as possible.
- ❑ We also want uniformity over the largest possible radius (R_{\max}).
- ❑ Can we make ONE heater work for the entire operating range of pressure and flow rate?
- ❑ **Strategy:** *fix the ratio of each heater power* from baseline optimal result (100 Torr, 50 slm) and scale this power distribution up and down with one input scaling.
 - This ratio can be done in hardware (e.g., filament density distribution, or resistance variation, etc.)
 - One zone control requires only one temperature sensor.

Optimizing Rmax (6-zone control)

100 Torr, 50 slm



It is only possible to get the inner 0.13 m radius within the design limits.

Rmax = 0.13 m

Rmax = 0.15 m

Optimizing T over the full radial span ($0 < r < 0.15$ m) results in a large region of the susceptor falling outside the design limits.

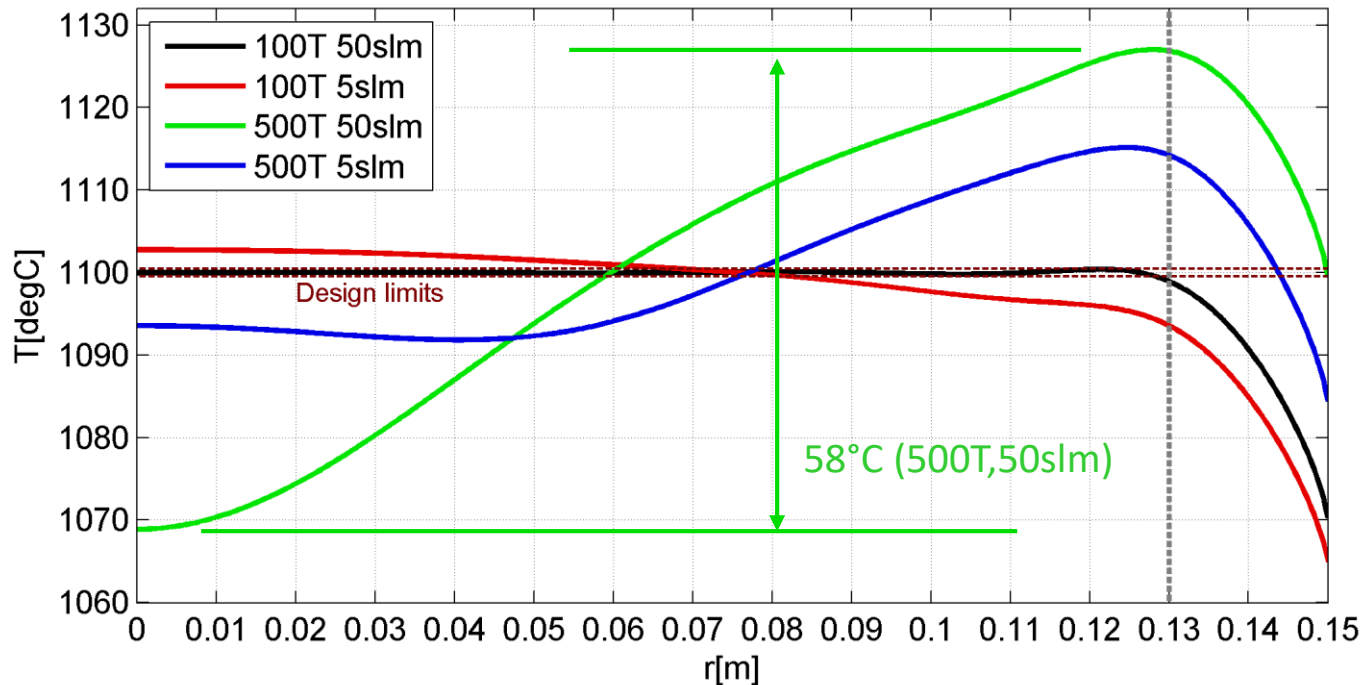
For remaining analysis we will only control the temperature for radius $r < 0.13$ m.

One-zone Control

- ❑ We found the “optimal” R_{max} to produce the largest area of temperature within design limits.
- ❑ Next we want to optimize the input flux distribution for different operating conditions.
- ❑ First we look at 1-zone control, then look at the improvement of increasing the number of independent control zones.

One Zone Control

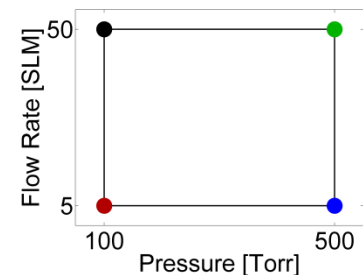
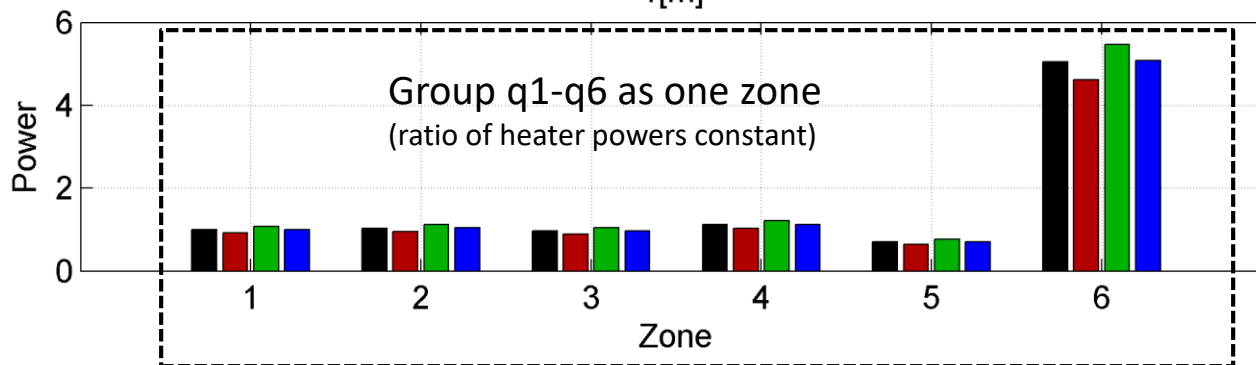
Temperature - 1-zone Control



In all cases the mean temperature optimized for $r < 0.13\text{m}$ and $T_{\text{ref}} = 1100^\circ\text{C}$

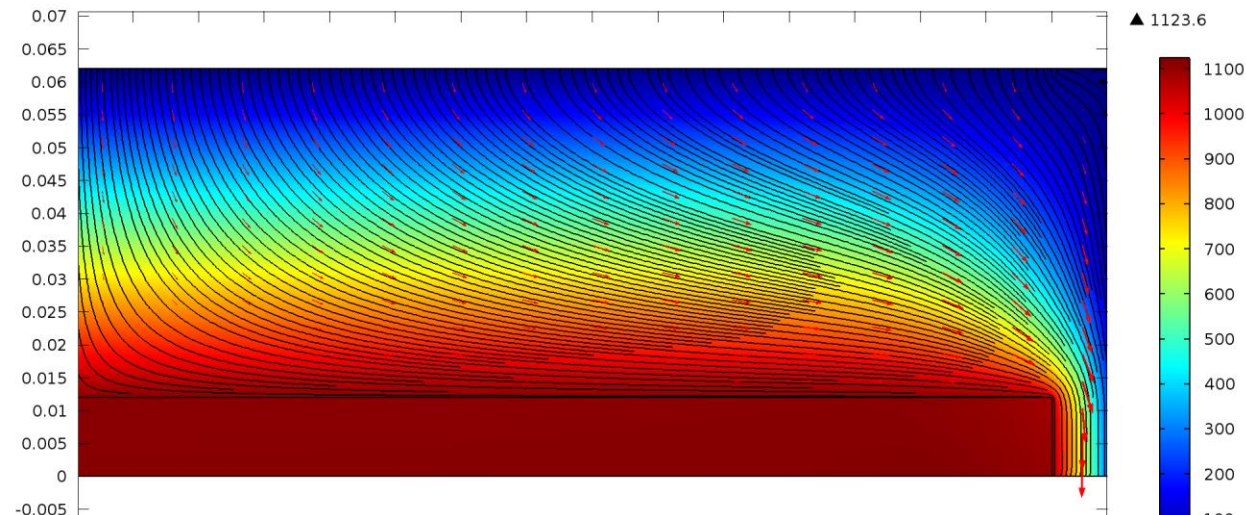
Except for the baseline case (100T, 50slm), the uniformity is poor.

High pressure is a problem. Look at the flows to see why.



Lower Pressure Flow fields (100 Torr)

T[degC], SLM=50, p=100 Torr, RPM=100

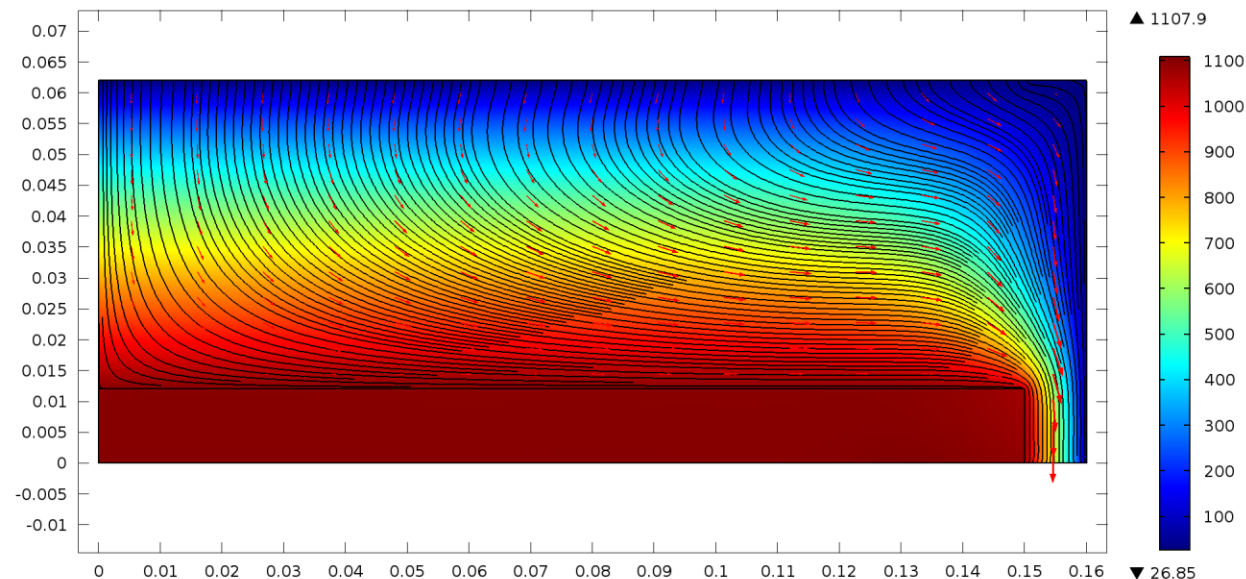


100 Torr, 50 slm



Baseline case.

T[degC], SLM=5, p=100 Torr, RPM=100



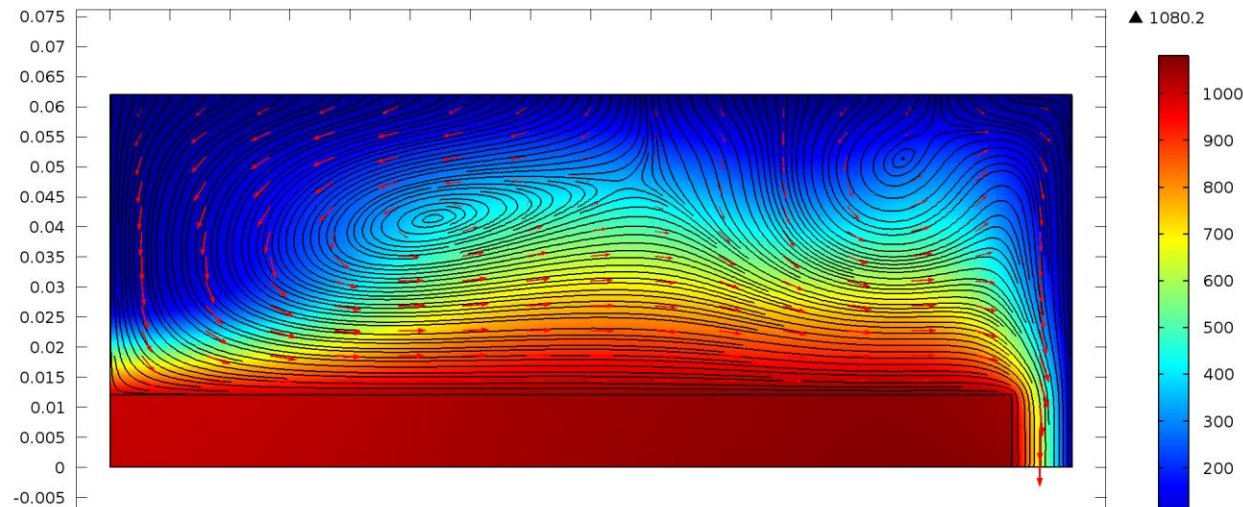
100 Torr, 5 slm



For slower flow we start to see some “lift” of the streamlines at larger radius.

Higher Pressure Flow fields (500 Torr)

T[degC], SLM=50, p=500 Torr, RPM=100

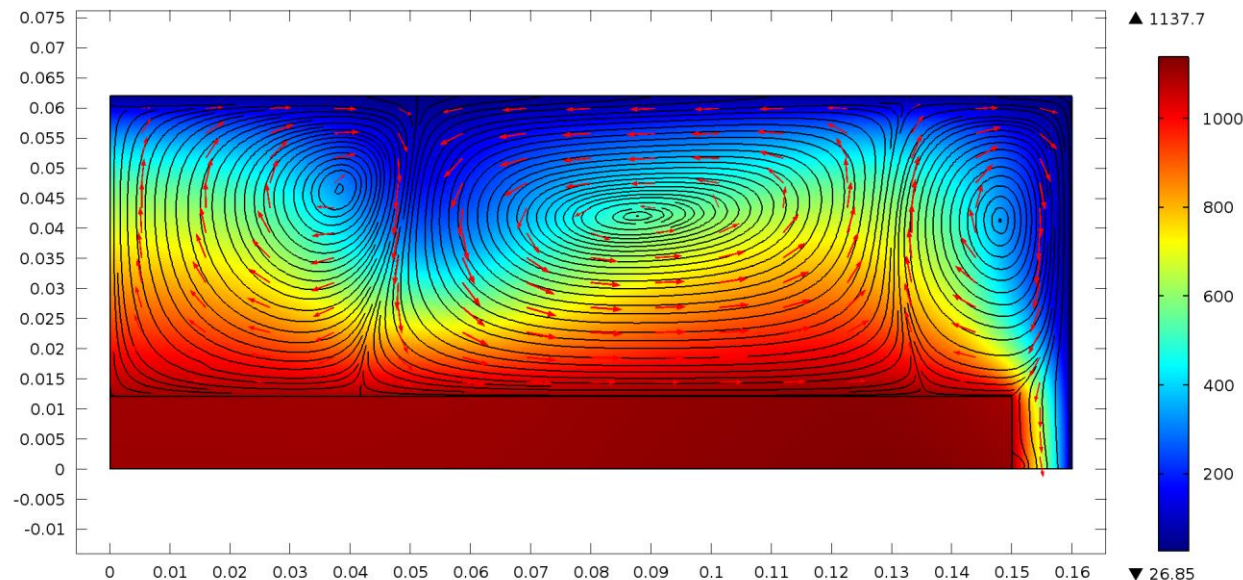


500 Torr, 50slm



Buoyancy driven recirculation is causing a significant redistribution of the convective losses.

T[degC], SLM=5, p=500 Torr, RPM=100



500 Torr, 5slm

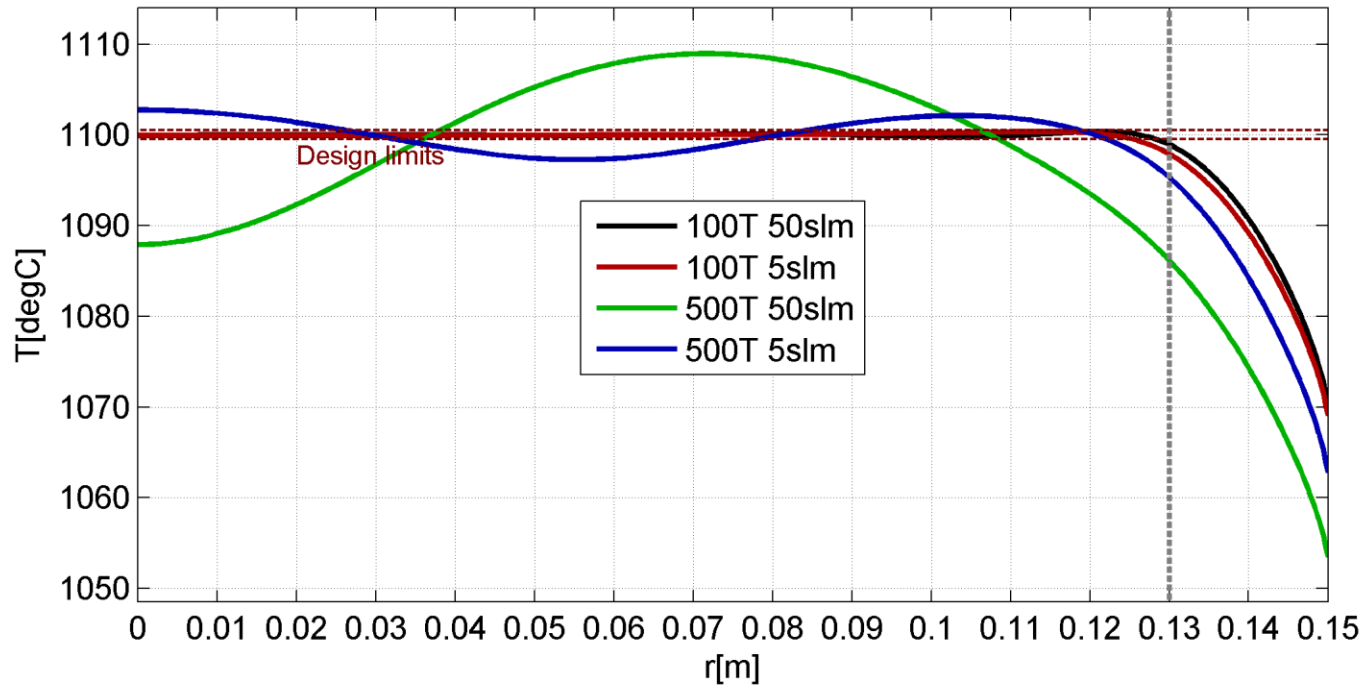


Buoyancy driven recirculation even more complex here.

1-zone control cannot work for this range of operating conditions.

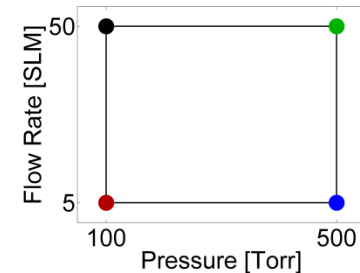
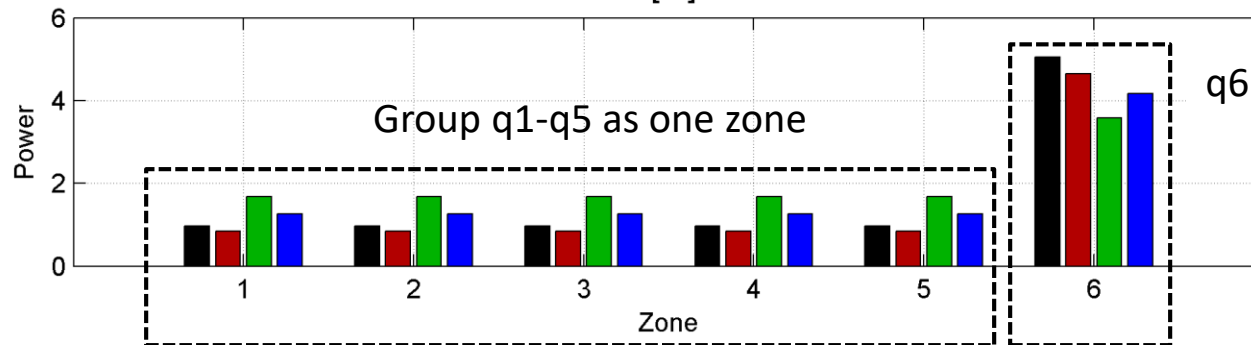
Two-zone Control

Temperature 2-zone Control

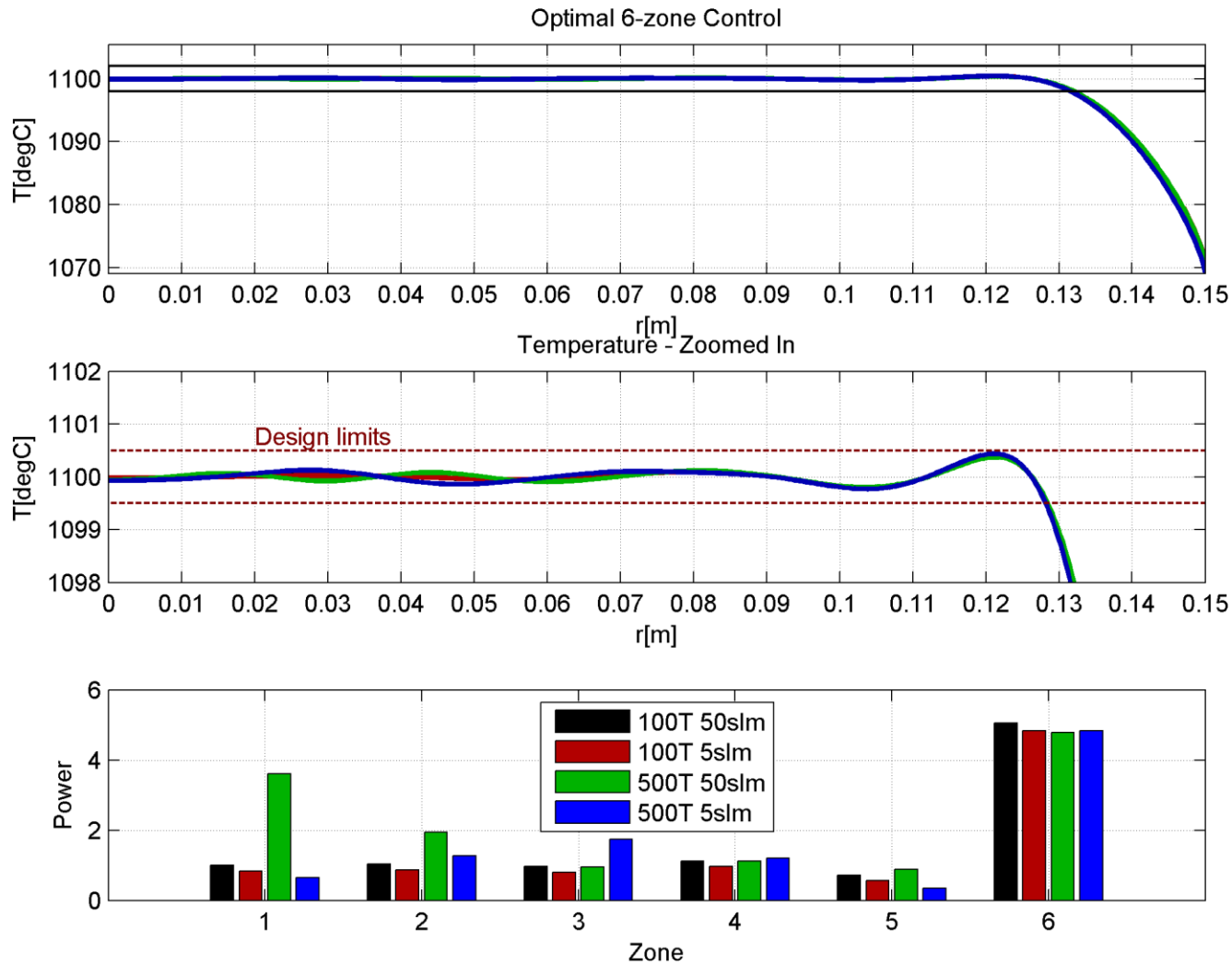


Much better, but still not within design limits.

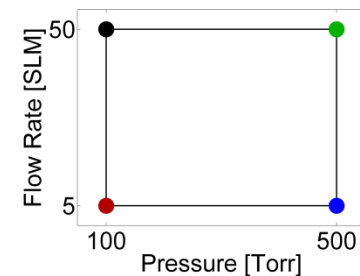
Both 100 Torr processes are close to being within the design limits.



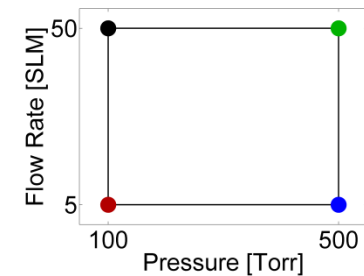
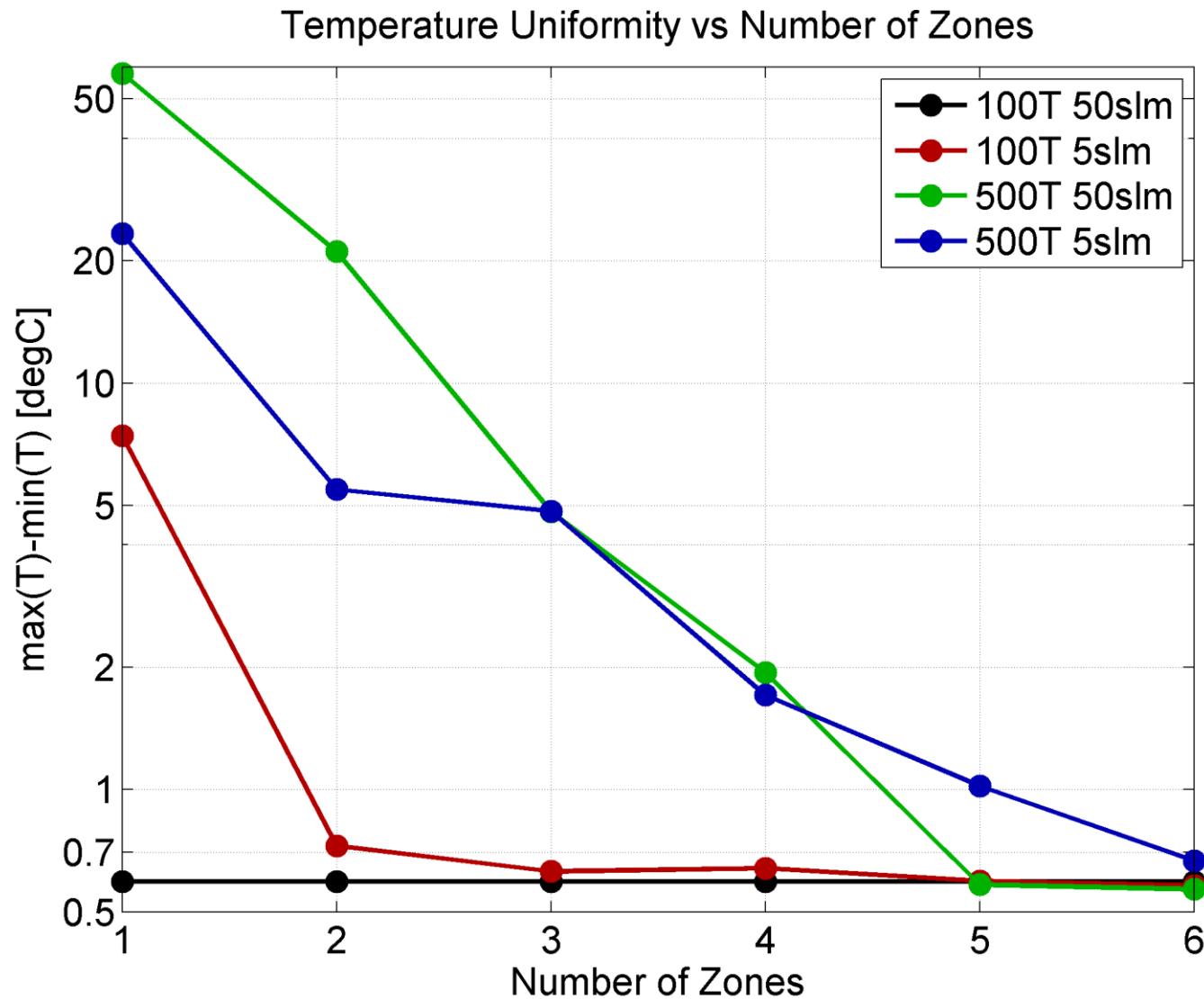
Six-zone Control



With Six Zones, the design specifications are met.

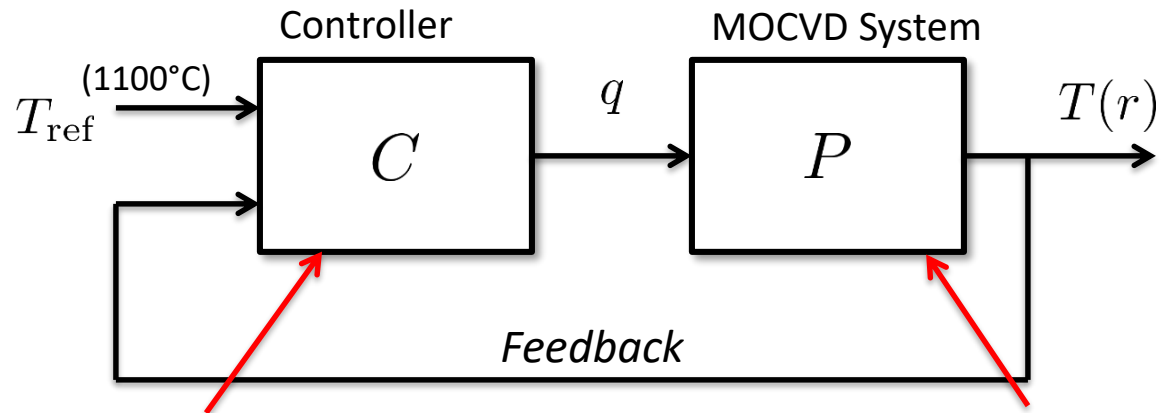


Temperature Uniformity vs Number of Control Zones



Implementation using Model-Based Control (MBC)

- ❑ The controller, C , adjusts the flux, q , to make the temperature T on the CVD surface uniform at the reference temperature, T_{ref} .

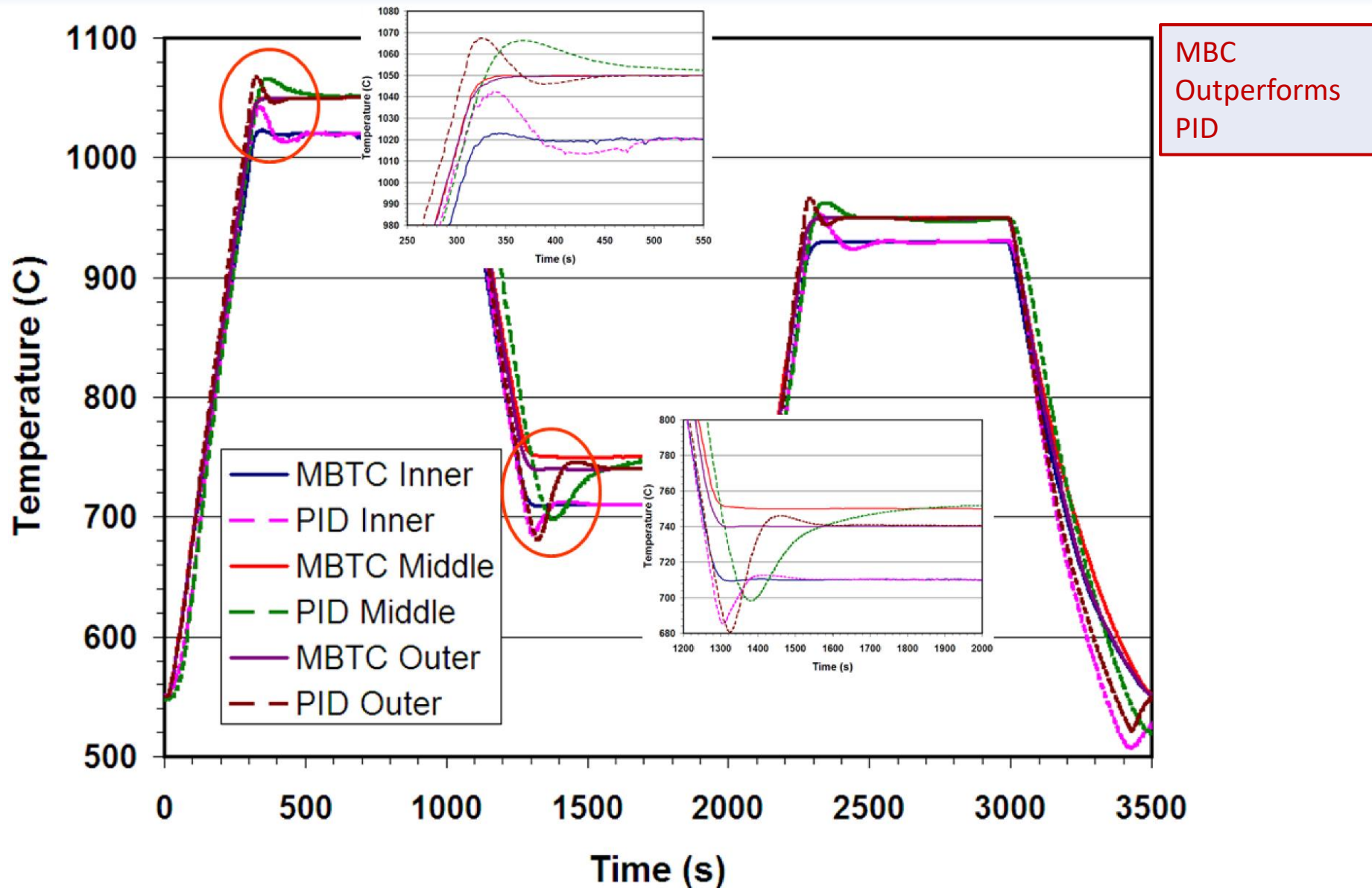


Control design tool \longleftrightarrow **Modeling tool**

- ❑ This is a form of the “inverse problem”.
(What inputs do I need to produce a given output?)
- ❑ Real-time feedback is a common method of dynamically solving this problem.

Here we focus on steady-state, but the same methods are used to solve the time-varying dynamic control problem (e.g., uniformity during temperature ramp, stabilization, etc.).

Dynamic Control Performance using Model-Based Control



W. E. Quinn, *Driving Down HB-LED Costs: Implementation of Process Simulation Tools and Temperature Control Methods for High Yield MOCVD Growth*, Final Technical Report DoE Grant DE-EE0003252.

Summary

- ❑ This study illustrates how modeling tools can be used together with control design tools to evaluate optimal closed-loop control performance of a system using Model-Based Control (MBC).
- ❑ In this particular study with a MOCVD system, after testing various multizone heater configurations, a six-zone control scheme was adopted with each heater being controlled independently.
- ❑ Temperature uniformity is much better than the specification over most of the area (0.7°C compared to 1°C specification).
- ❑ Fewer independent heater zones are needed if uniformity requirement is relaxed slightly (4 zones sufficient for $\pm 1^\circ\text{C}$).
- ❑ Additionally, the results point to a need to eliminate “roll cells” in the flow, either by changing the geometry, increasing the flow rate, or increasing the rotation rate.

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